

Ion Slip Effect on The Flow of a Dusty Fluid Through a Circular Pipe

Hazem Ali Attia*

*Department of Mathematics, College of Science, King Saud University (Al-Qasseem Branch),
P.O. Box 237, Buraidah 81999, KSA*

(Manuscript Received May 24, 2006; Revised January 10, 2007; Accepted January 10, 2007)

Abstract

In this paper, the transient flow of a dusty viscous incompressible electrically conducting fluid through a circular pipe is studied taking the ion slip into consideration. A constant pressure gradient in the axial direction and a uniform magnetic field directed perpendicular to the flow direction are applied. The particle-phase is assumed to behave as a viscous fluid. A numerical solution for the governing equations is obtained using finite differences.

1. Introduction

The flow of a dusty and electrically conducting fluid through a circular pipe in the presence of a transverse magnetic field has important applications such as magnetohydrodynamic generators, pumps, accelerators, and flowmeters. The performance and efficiency of these devices are influenced by the presence of suspended solid particles in the form of ash or soot as a result of the corrosion and wear activities and/or the combustion processes in MHD generators and plasma MHD accelerators. When the particle concentration becomes high, mutual particle interaction leads to higher particle-phase viscous stresses and can be accounted for by endowing the particle phase by the so-called particle-phase viscosity. There have been many articles dealing with theoretical modelling and experimental measurements of the particle-phase viscosity in a dusty fluid (Soo, 1969; Gidaspow et al., 1989; Grace, 1982; Sinclair and Jackson, 1989).

The flow of a conducting fluid in a circular pipe

has been investigated by many authors (Gadiraju et al., 1992; Dube and Sharma, 1975; Ritter and Peddieson, 1977; Chamkha, 1994). (Gadiraju et al., 1992) investigated steady two-phase vertical flow in a pipe. (Dube and Sharma, 1975) and (Ritter and Peddieson, 1977) reported solutions for unsteady dusty-gas flow in a circular pipe in the absence of a magnetic field and particle-phase viscous stresses. (Chamkha, 1994) obtained exact solutions which generalize the results reported in (Dube and Sharma, 1975; Ritter and Peddieson, 1977) by the inclusion of the magnetic and particle-phase viscous effects. The heat transfer characteristics of circular pipe flow was studied by many researchers (Yoon et al., 2002; Kim, 2002; Kim, 2003). It should be noted that in the above studies the Hall current as well as the ion slip effects are ignored. In fact, the Hall effect is important when the Hall parameter, which is the ratio between the electron-cyclotron frequency and the electron-atom-collision frequency, is high. This happens when the magnetic field is high or when the collision frequency is low (Crammer and Pai, 1973; Sutton and Sherman, 1965). Furthermore, the masses of the ions and electrons are different and, in turn, their motions will be different. Usually, the diffusion velocity of electrons is larger

*Corresponding author. Tel.: +009 66 6 3826928, Fax.: +00966 63800911
E-mail address: ah1113@yahoo.com

than that of ions and, as a first approximation, the electric current density is determined mainly by the diffusion velocity of the electrons. However, when the electromagnetic force is very large (such as in the case of strong magnetic field), the diffusion velocity of the ions may not be negligible (Crammer and Pai, 1973; Sutton and Sherman, 1965). If we include the diffusion velocity of ions as well as that of electrons, we have the phenomena of ion slip. In the above mentioned work, the Hall and ion slip terms were ignored in applying Ohm's law, as they have no marked effect for small and moderate values of the magnetic field. However, the current trend for the application of magnetohydrodynamics is towards a strong magnetic field, so that the influence of the electromagnetic force is noticeable under these conditions, and the Hall current as well as the ion slip are important; they have a marked effect on the magnitude and direction of the current density and consequently on the magnetic-force term (Crammer and Pai, 1973; Sutton and Sherman, 1965).

In the present study, the unsteady flow of a dusty electrically conducting fluid through a circular pipe is investigated considering the ion slip. The carrier fluid is assumed viscous, incompressible and electrically conducting. The particle phase is assumed to be incompressible pressureless and electrically non-conducting. The flow in the pipe starts from rest through the application of a constant axial pressure gradient. The governing momentum equations for both the fluid and particle-phases are solved numerically using the finite difference approximations. The effect of the magnetic field, the Hall current, the ion slip and the particle-phase viscosity on the velocity distributions of the fluid and particle-phases is reported.

2. Governing equations

Consider the unsteady, laminar, axisymmetric horizontal flow of a dusty conducting fluid through an infinitely long pipe of radius "d" driven by a constant pressure gradient. A uniform magnetic field is applied perpendicular to the flow direction. The Hall current and the ion slip are taken into consideration and the magnetic Reynolds number is assumed to be very small and consequently the induced magnetic field is neglected (Crammer and Pai, 1973; Sutton and Sherman, 1965). We assume that both phases behave as viscous fluids and that the volume fraction of suspended particles is finite and constant (Chamkha, 1994).

Taking into account these and the previously mentioned assumptions, the governing momentum equations can be written as

$$\rho \frac{\partial V}{\partial t} = -\frac{\mu \partial}{r \partial r} \left(r \frac{\partial V}{\partial r} \right) + \frac{\rho_p \phi}{1-\phi} N(V_p - V) - \frac{\sigma B_0^2 (1 + \beta_i \beta_e) V}{(1 + \beta_i \beta_e)^2 + \beta_e^2} \quad (1)$$

$$\rho_p \frac{\partial V_p}{\partial t} = -\frac{\mu_p}{r} \frac{\partial}{\partial r} \left(r \frac{\partial V_p}{\partial r} \right) + \rho_n N(V - V_p) \quad (2)$$

where t is time, r is the distance in the radial direction, V is the fluid-phase velocity, V_p is the particle-phase velocity, ρ is the fluid-phase density, ρ_p is the particle-phase density, $\partial P / \partial z$ is the fluid pressure gradient, ϕ is the particle-phase volume fraction, N is a momentum transfer coefficient (the reciprocal of the relaxation time, the time needed for the relative velocity between the phases to reduce e^{-1} of its original value (Chamkha, 1994)), σ is the fluid electrical conductivity, $\beta_e = \sigma \gamma B_0$ is the Hall parameter, γ is the Hall factor (Crammer and Pai, 1973; Sutton and Sherman, 1965), B_0 is the magnetic induction, β_i is the ion slip parameter, μ_p is the particle-phase viscosity which is assumed constant, and μ is the viscosity of the fluid.

It should be pointed out that the particle-phase pressure is assumed negligible and that the particles are being dragged along with the fluid-phase.

The initial and boundary conditions of the problem are given as

$$V(r, 0) = 0, \quad V_p(r, 0) = 0, \quad (3a)$$

$$V(d, t) = 0, \quad V_p(d, t) = 0$$

$$\frac{\partial V(0, t)}{\partial r} = 0, \quad \frac{\partial V_p(0, t)}{\partial r} = 0, \quad (3b)$$

where "d" is the pipe radius.

Equations (1)-(3) constitute an initial-value problem which can be made dimensionless by introducing the following dimensionless variables and parameters

$$\bar{r} = \frac{r}{d}, \quad \bar{t} = \frac{t \mu}{\rho d^2}, \quad G_0 = -\frac{\partial P}{\partial z}, \quad k = \frac{\rho_p \phi}{\rho(1-\phi)},$$

$$\bar{V}(r, t) = \frac{\mu V(r, t)}{G_0 d^2}, \quad \bar{V}_p(r, t) = \frac{\mu V_p(r, t)}{G_0 d^2},$$

$\alpha = Nd^2 \rho / \mu$ is the inverse Stoke's number,

$\beta = \mu_p / \mu$ is the viscosity ratio,

$H_a = B_o d \sqrt{\sigma / \mu}$ is the Hartmann number.

By introducing the above dimensionless variables and parameters as well as the expression of the fluid viscosity defined above, Eqs. (1)~(3) can be written as (the bars are dropped),

$$\frac{\partial V}{\partial t} = 1 + \frac{\partial^2 V}{\partial r^2} + \frac{1}{r} \frac{\partial V}{\partial r} + \kappa \alpha (V_p - V) - \frac{H_a^2 (1 + \beta_i \beta_e) V}{(1 + \beta_i \beta_e)^2 + \beta_e^2} \tag{4}$$

$$\frac{\partial V_p}{\partial t} = \beta \left(\frac{\partial^2 V_p}{\partial r^2} + \frac{1}{r} \frac{\partial V_p}{\partial r} \right) + \alpha (V - V_p) \tag{5}$$

$$\begin{aligned} V(r, 0) &= 0, & V_p(r, 0) &= 0, \\ \frac{\partial V(0, t)}{\partial r} &= 0, & \frac{\partial V_p(0, t)}{\partial r} &= 0, \\ V(1, t) &= 0, & V_p(1, t) &= 0 \end{aligned} \tag{6a}$$

The volumetric flow rates and skin-friction coefficients for both the fluid and particle phases are defined, respectively, as (Chamkha, 1994)

$$\begin{aligned} Q &= 2 \int_0^1 \pi r V(r, t) dr, & Q_p &= 2 \int_0^1 \pi r V_p(r, t) dr \\ C &= -\frac{\partial V(1, t)}{\partial r}, & C_p &= -\beta k \frac{\partial V_p(1, t)}{\partial r} \end{aligned} \tag{7}$$

3. Results and discussion

Equations (4) and (5) represent a coupled system of partial differential equations which are solved numerically under the initial and boundary conditions (6), using the finite difference approximations. The Crank-Nicolson implicit method (Mitchell and Griffiths, 1980; Evans et al., 2000) is used at two successive time levels. Finally, the resulting block tridiagonal system is solved using the generalized Thomas algorithm (Mitchell and Griffiths, 1980; Evans et al., 2000). Computations have been made for $\alpha=1$ and $k=10$. Grid-independence studies show that the computational domain $0 < t < \infty$ and $0 < r < 1$ can be divided into intervals with step sizes

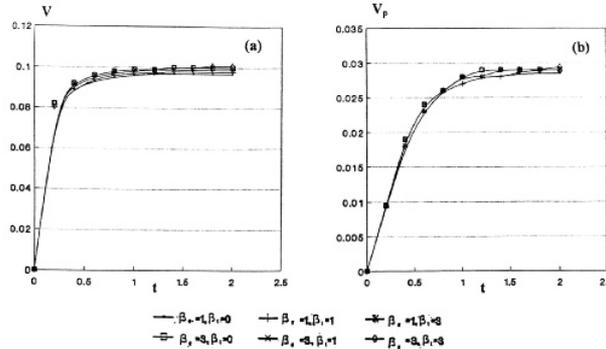


Fig. 1. Effect of the parameters β_e and β_i on the time evolution of: (a) V at $r=0$ and (b) V_p at $r=0$.

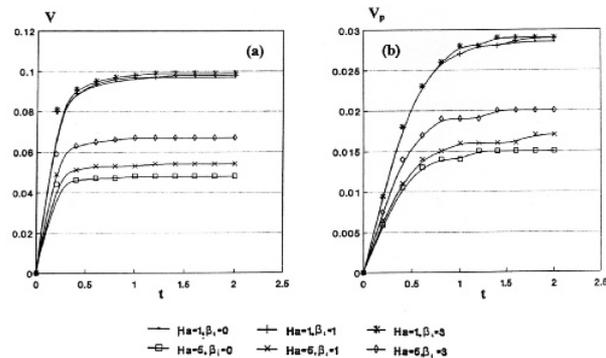


Fig. 2. Effect of the parameters H_a and β_i on the time evolution of: (a) V at $r=0$ and (b) V_p at $r=0$.

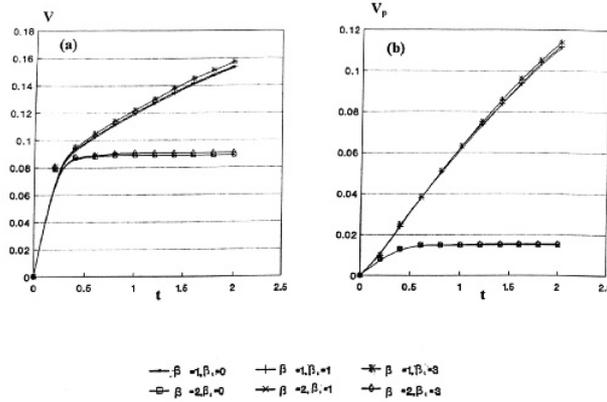


Fig. 3. Effect of the parameters β and β_i on the time evolution of: (a) V at $r=0$ and (b) V_p at $r=0$.

$\Delta t = 0.0001$ and $\Delta y = 0.005$ for time and space respectively. It should be mentioned that the results obtained herein reduce to those reported by (Dube and Sharma, 1975; Ritter and Peddieson, 1977) when $Ha = 0$ and $\beta = 0$. Also, the steady state solutions reported by Chamkha [8] in the absence of the Hall current and ion slip are reproduced by setting $\beta_e = 0$ in the present results. These comparisons give confidence in the accuracy and correctness of the solutions.

Figures 1a and b present the time evolution of the velocity of the fluid V and dust particles V_p at the center of the pipe, respectively, for various values of the ion slip parameter β_i and the Hall parameter β_e and for $H_a = 1$ and $\beta = 0.5$. Both V and V_p increase with time and V reaches the steady state faster than V_p for all values of β_e and β_i . It is clear from the figures that increasing β_e or β_i increases both V and V_p while its effect on their steady state times can be neglected. This is due to the decrease in the effective conductivity which reduces the damping magnetic force on V .

Figures 2a and b present the time evolution of the velocity of the fluid V and dust particles V_p at the center of the pipe, respectively, for various values of the ion slip parameter β_i and the Hartmann number H_a and for $\beta_e = 1$ and $\beta = 0.5$. It is clear that increasing H_a decreases V and V_p and their steady state times for all values of β_i due to the increase in the damping magnetic force. The figures indicate also that the effect of β_i on V and V_p becomes more pronounced for higher values of H_a .

Table 1. The Steady State Values of Q , Q_p , C , C_p for Various Values of β_i and β and for $H_a = 1$.

B=0	$\beta_i=0$	$\beta_i=1$	$\beta_i=3$
Q	0.2120	0.2142	0.2178
Q_p	0.1569	0.1583	0.1607
C	0.3697	0.3721	0.3763
C_p	0	0	0

B=0.5	$\beta_i=0$	$\beta_i=1$	$\beta_i=3$
Q	0.1391	0.1401	0.1419
Q_p	0.0363	0.0366	0.0370
C	0.2786	0.2798	0.2819
C_p	0.2070	0.2085	0.2108

B=1	$\beta_i=0$	$\beta_i=1$	$\beta_i=3$
Q	0.1286	0.1295	0.1310
Q_p	0.0193	0.0195	0.0197
C	0.2675	0.2685	0.2704
C_p	0.2196	0.2210	0.2234

Table 2. The Steady State Values of Q , Q_p , C , C_p for Various Values of β_i and β and for $H_a = 5$.

B=0	$\beta_i=0$	$\beta_i=1$	$\beta_i=3$
Q	0.0929	0.1057	0.1358
Q_p	0.0742	0.0835	0.1051
C	0.2246	0.2415	0.2797
C_p	0	0	0

B=0.5	$\beta_i=0$	$\beta_i=1$	$\beta_i=3$
Q	0.0736	0.0816	0.0995
Q_p	0.0193	0.0214	0.0260
C	0.1944	0.2056	0.2294
C_p	0.1159	0.1274	0.1525

B=1	$\beta_i=0$	$\beta_i=1$	$\beta_i=3$
Q	0.0705	0.0779	0.0939
Q_p	0.0106	0.0117	0.0142
C	0.1909	0.2015	0.2234
C_p	0.1264	0.1384	0.1645

Figures 3a and b present the time evolution of the velocity of the fluid V and dust particles V_p at the center of the pipe, respectively, for various values of

the ion slip parameter β_i and the viscosity ratio β and for $\beta_e = 1$ and $H_a = 1$. The figures indicate that increasing β decreases both V and V_p and their steady state times for all values of β_i . The effect of the parameter β_i on V and V_p is more apparent for higher values of the parameter β .

Tables 1 and 2 present the steady state values of the fluid-phase volumetric flow rate Q , the particle-phase volumetric flow rate Q_p , the fluid-phase skin friction coefficient C , and the particle-phase skin friction coefficient C_p for various values of the parameters β_i and β and for $H_a = 1$ and $H_a = 5$, respectively. In these tables $\beta_e = 1$. It is shown that increasing β_i increases Q , Q_p , C , and C_p for all values of β and H_a . Also, increasing β decreases Q , Q_p , and C , but increases C_p for all values of β_i and H_a . It is clear also from the tables that the effect of β on the quantities Q , Q_p , C and C_p is more pronounced for higher values of H_a , while the effect of β_i on these quantities is more apparent for smaller values of H_a .

4. Conclusions

The transient MHD flow of a particulate suspension in an electrically conducting fluid through a circular pipe is studied considering the ion slip. The governing partial differential equations are solved numerically using finite differences. The effect of the magnetic field parameter H_a , the Hall parameter β_e , the ion slip parameter β_i , and the particle-phase viscosity β on the transient behavior of the velocity, volumetric flow rates, and skin friction coefficients of both fluid and particle-phases is studied. It is shown that increasing the magnetic field or the viscosity ratio decreases the fluid and particle velocities, while increasing the Hall parameter or the ion slip parameter increases both velocities. It is found that, the effect of the ion slip on the fluid and particle velocities is more apparent for higher values of the magnetic field or the viscosity ratio.

References

Crammer, K. R., Pai, S. -I., 1973, Magnetofluid Dynamics for Engineers and Applied Physicists, Mc-

Graw-Hill, New York.

Chamkha, A. J., 1994, "Unsteady Flow of a Dusty Conducting Fluid Through a Pipe," *Mechanics Research Communications*, Vol. 21, No. 3, pp. 281-286.

Dube, S. N., Sharma, C. L., 1975, "A Note on Unsteady Flow of a Dusty Viscous Liquid in a Circular Pipe," *J. Phys. Soc. Japan*, Vol. 38, No. 1, pp. 298-310.

Evans, G. A., Blackledge, J. M., Yardley, P. D., 2000, *Numerical Methods for Partial Differential Equations*, Springer Verlag, New York.

Grace, J. R., 1982, *Fluidized-Bed Hydrodynamic*, Handbook of Multiphase Systems, G. Hetsoroni, Ed., Ch. 8.1, McGraw-Hill, New York.

Gidaspow, D., 1986, "Hydrodynamics of Fluidization and Heat Transfer: Super Computer Modeling," *Appl. Mech. Rev.*, Vol. 39, pp. 1-23.

Gadiraju, M., Peddieson, J., Munukutla, S., 1992, "Exact Solutions for Two-Phase Vertical Pipe Flow," *Mechanics Research Communications*, Vol. 19, No. 1, pp. 7-13.

Mitchell A. R., Griffiths, D. F., 1980, *The Finite Difference Method in Partial Differential Equations*, John Wiley & Sons, New York.

Ritter, J. M., Peddieson, J., 1977, "Transient Two-Phase Flows in Channels and Circular Pipes," *Proc. 1977 the Sixth Canadian Congress of Applied Mechanics*.

Yoon, S. H., Oh, Cheol, Choi, J. H., "A Study of the Heat Transfer Characteristics of a Self-Oscillating Heat Pipe," *KSME International Journal*, Vol. 16, No. 3, pp. 354-362, 2002.

Kim, D., "Improved Convective Heat Transfer Correlations for Two-Phase Two-Component Pipe," *KSME International Journal*, Vol. 16, No. 3, pp. 403-422, 2002.

Kim, W. T., Hong, K. H., Jhon, M. S., VanOsdol, J. G., Smith, D. H., "Forced Convection in a Circular Pipe with a Partially Filled Porous Medium," *KSME International Journal*, Vol. 17, No. 10, pp. 1583-1596, 2003.

Sutton, G. W., Sherman, A., 1965, *Engineering Magnetohydrodynamics*, McGraw-Hill, New York.

Soo, S. L., 1969, "Pipe Flow of Suspensions," *Appl. Sci. Res.*, Vol. 21, pp. 68-84.

Sinclair, J. L., Jackson, R., 1989, "Gas-Particle Flow in a Vertical Pipe with Particle-Particle Interactions," *AICHE J.*, Vol. 35, pp. 1473-1486.